

Institute for Polymer Research  
27<sup>th</sup> Annual Symposium

Symposium documents for

**Kerry Li**

**Abstract**

**Presentation**

## **Extrusion and fibre spinning of Nylon-6,6 / supercritical CO<sub>2</sub> mixture**

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### **Abstract:**

A novel technical to spin nylon fibre was developed: Addition of supercritical CO<sub>2</sub> to nylon melts and spinning those mixtures under different conditions were performed. CO<sub>2</sub> works co-ordinately with thermal to disrupt nylon-6,6 inter-chain hydrogen bond. In sequent, the intended improvement in stretching along with tensile properties of nylon fibres was evaluated.

As an elementary exploration, the rheological behaviour of nylon-6,6 / supercritical CO<sub>2</sub> mixture was explored through a custom extrusion. Results indicate that the CO<sub>2</sub> as a plasticizer reduce the bulk shear viscosity. The combined effects of temperature and hydrostatic pressure on shear viscosity were investigated accordingly.

### **Introduction.**

Nylon-6,6 is one of semi-crystalline polymers with very polar characteristic amide groups in the symmetrical backbone chain. The amide group  $\text{-(CO-NH)-}$  provides high density hydrogen bonding between polyamide chains, giving nylon high strength at elevated temperatures, toughness at low temperatures, combined with its other properties, such as stiffness, wear and abrasion resistance, low friction coefficient and good chemical resistance. These properties have made nylons the strongest of all man-made fibers in common use.

Mechanical, thermal and optical properties of fibers are strongly affected by orientation and crystallinity. Basically, higher fiber orientation and crystallinity will produce better properties. In order to achieve desirable properties through molecular orientation and crystallinity, two-step melt spinning, comprised of spinning and drawing, is considered to be the conventional method to manufacture nylon filaments.

Multiple drawing stages were invented to achieve high levels of orientation. The mechanism is to obtain relaxation allow for drawing in the later stages. However, the tensile strength of nylon-6,6 produced through this technical is less than 1.0Gpa and much lower than their theoretical strength. The highest orientation and crystallinity are hard to achieve by this technical since the high density of hydrogen bond in nylon crystal stem restrict the further drawing. Therefore, disruption of the hydrogen bonds is necessary to obtain further stretching and improved tensile properties.

Lewis acid-base complexion, such as carbon dioxide interact with carbonyls, was found to be able to scission the hydrogen bond in nylon-6,6 inter-chain. Most recently, a technique to draw polymer in high pressure gases has been presented in this purpose. The drawing process has been monitor in specified temperature and pressure range. Also the gas or liquids act mostly as plasticizer in drawing process. In those attempts, the use of

scCO<sub>2</sub> only evaluates the ability of scCO<sub>2</sub> to plasticize amorphous fibres. Meanwhile, the discussion of interaction of carbon dioxide with electron donor species (e.g. carbonyls) is absent.

Ideally, if we are able to disassociate inter-chain hydrogen bond of nylon before drawing and recover them after drawing, the highest stretching may be achieved, as well as the tensile strength. In our spinning and drawing approach, the addition of CO<sub>2</sub> during extrusion of nylon-6,6 melts presents complex effects attributed to both chemical structure ( interact with carbonyls) and supermolecular (plasticize). The reduction of bulk shear viscosity rally with the weakness of polymer hydrogen bond may facilitate higher degree of stretching when spinning, the existing of CO<sub>2</sub> in subsequent drawing process function as plasticizer which promote further stretching. The CO<sub>2</sub> selected as a media during process leave no trace in the end, the whole process is simple and environmental benign.

In order to estimate the plasticize performance of scCO<sub>2</sub>, a custom extrusion process designed to study the mixing and rheological behaviour in a systematic manner.

### **Experimental:**

The viscosity behavior of nylon-6,6 / supercritical CO<sub>2</sub> mixture was studied in a custom extrusion process, see Diagram 2.; A wedge die was used to connect with extruder to measure shear viscosity, the following formula apply in this measurement:

$$\Delta P = \frac{K}{\tan \theta} \left( \frac{6Q}{W} \frac{2n+1}{3n} \right)^n \left[ \frac{1}{2n} \left( \frac{1}{h_2^{2n}} - \frac{1}{h_0^{2n}} \right) + \frac{1}{W(2n-1)} \left( \frac{1}{h_2^{2n-1}} - \frac{1}{h_0^{2n-1}} \right) \right]$$

$$\eta = K \left( \frac{2n+1}{3n} \right) \left( \frac{6Q}{Wh^2} \right)^{n-1}$$

The spinning and drawing process show in Diagram 1. A custom high-pressure chamber will be used to avoid the foam in some instance. The design of chamber shows in Picture 1.

### **Results and discussion:**

The pressure, gas uptake and temperature effects on bulk shear viscosity shows in plot1, 2,3 respectively:

Spinning and drawing of mixture is ongoing, some spinning results show in plot 4,5,6:

## Schematic diagram of the continuous-draw apparatus

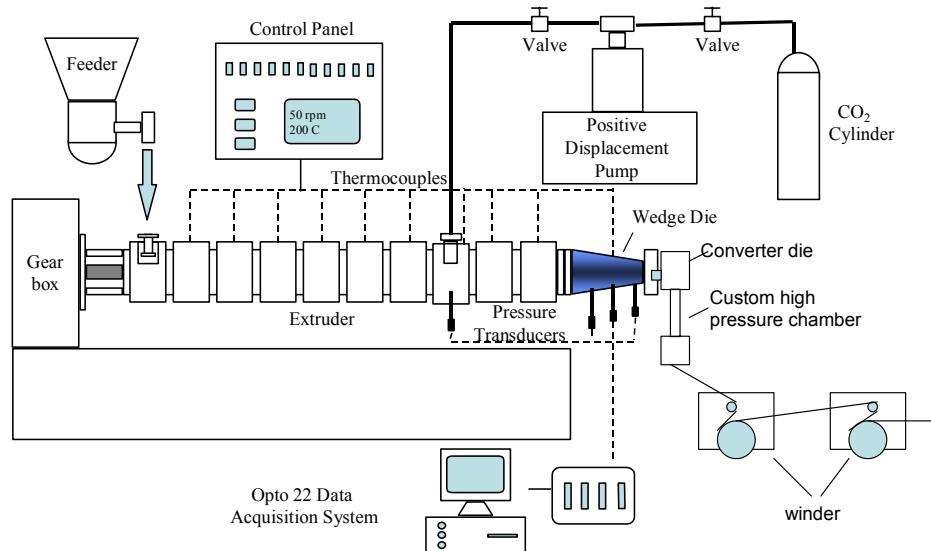
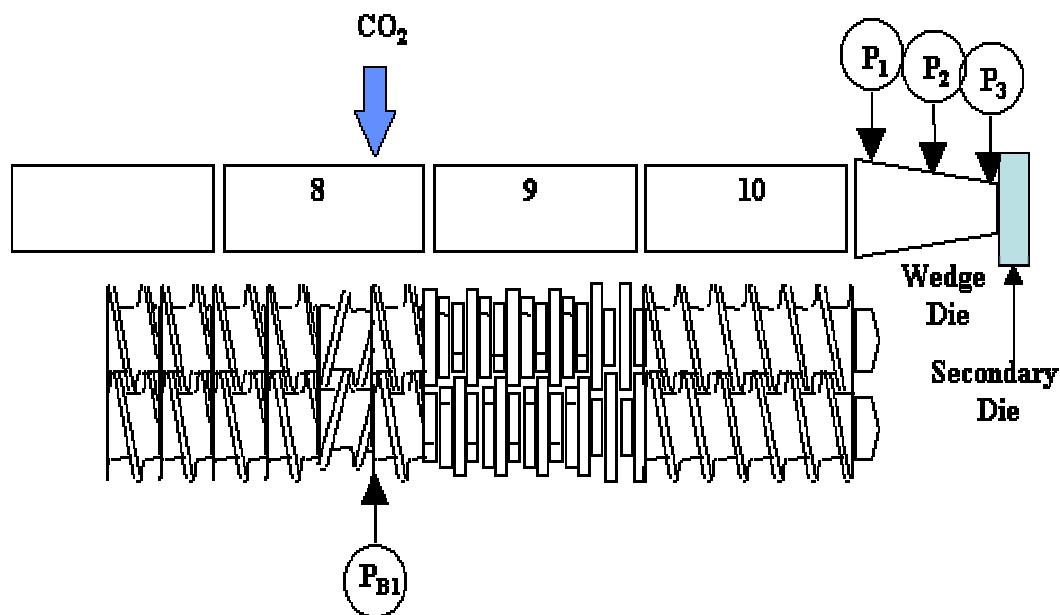
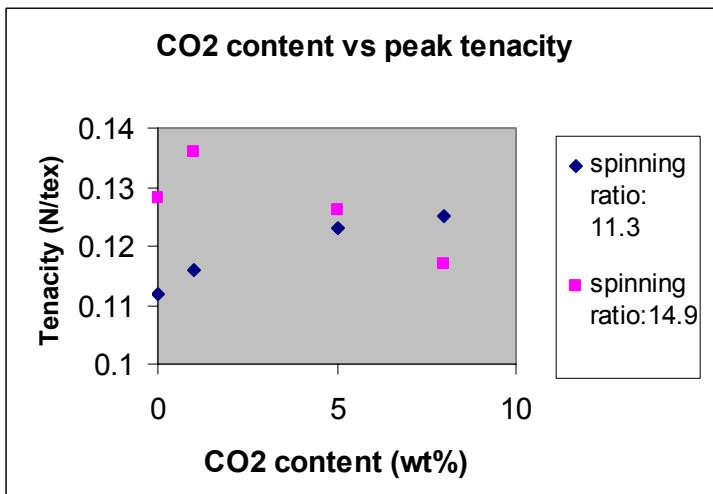
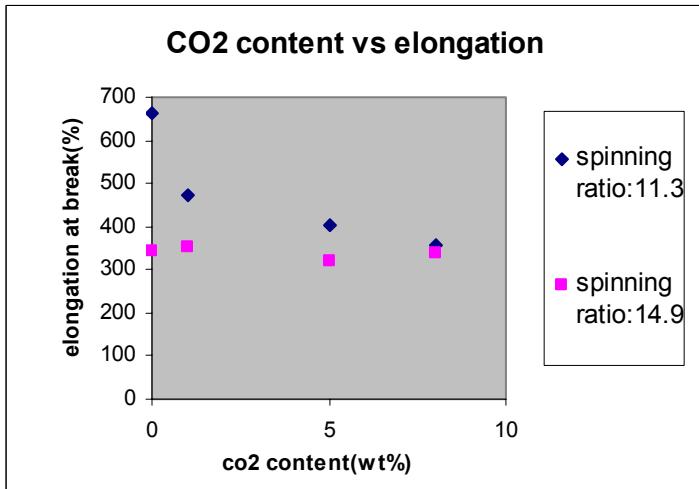
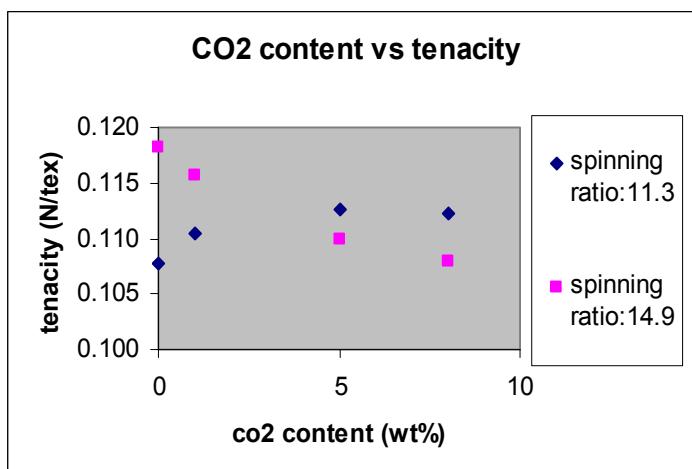


Diagram 2: Screw configuration

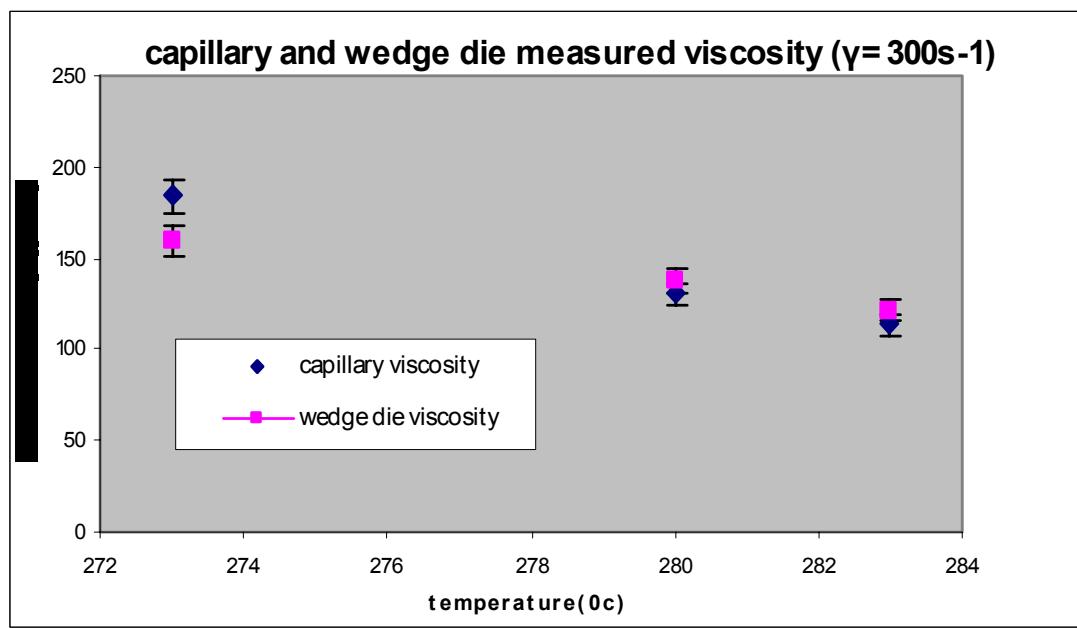
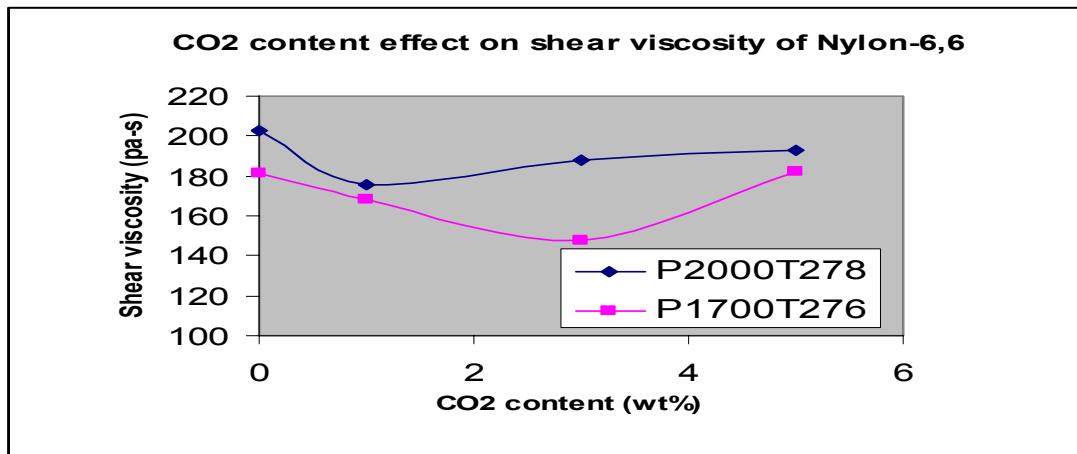
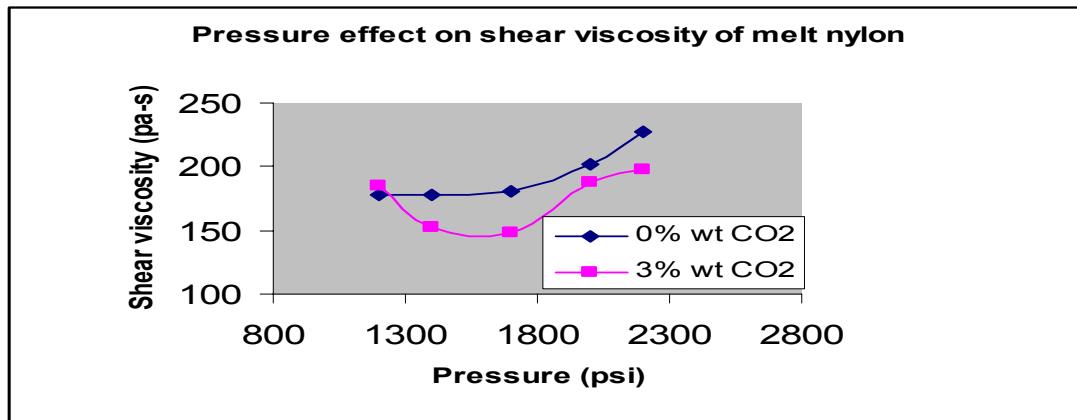


Plot 4,5,6: spinning results

Pic.1. high-pressure chamber



**Plot 1,2,3: The pressure, co<sub>2</sub> uptake and temperature effects to shear viscosity**



# Extrusion and fiber spinning of Nylon-6,6 / supercritical CO<sub>2</sub> mixtures

Presented by: Ziqiang Li  
Supervisor: C. Tzoganakis

IPR Symposium: May 18, 2005

## Content

- Objective
- Introduction
- Motivation and design concepts
- Preliminary experiments
- Extrusion of PA-6,6 / ScCO<sub>2</sub> mixture
- Filament spinning of PA-6,6 and mixture
- Conclusions
- Acknowledgement

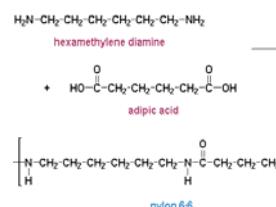
## Objective

- Investigate the effects of supercritical CO<sub>2</sub> on nylon-6,6 viscosity:
  - Prepare the supercritical CO<sub>2</sub> / nylon-6,6 mixture in extruder, on-line measure the effect of T,P,CO<sub>2</sub> content ,shear rate to shear viscosity via connected wedge die.
- Implement the spinning and drawing of supercritical CO<sub>2</sub> / nylon-6,6:
  - Spinning supercritical CO<sub>2</sub> / nylon-6,6 mixture or / and in custom chamber.
  - Investigate the effect of uptake of CO<sub>2</sub> to filament's mechanic properties ( tenacity, strength).

## Introduction:

### NYLON-6,6:

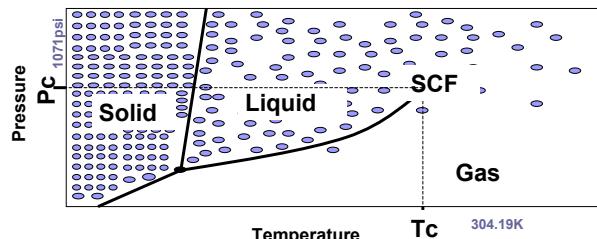
- Very polar characteristic amide groups in the symmetrical backbone chain



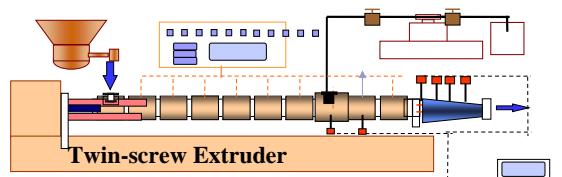
- ✓ High density of H-bond
- ✓ Semi - crystalline
- ✓ Good mechanical, thermal properties
- ✓ High DR under high temperature and moisture

## Introduction:

- Supercritical Fluids
  - A fluid is supercritical when its temperature and pressure are higher than their critical point values ( T<sub>c</sub> , P<sub>c</sub>).
- Supercritical Carbon Dioxide



## Introduction: Extrusion of PA-66 / ScCO<sub>2</sub>:



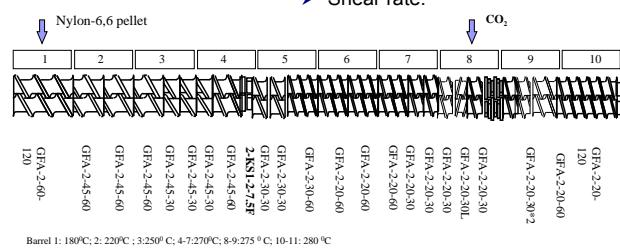
- Avoid degradation
- Maintenance high pressure
- Well mixing, avoid pressure fluctuate.
- Avoid back flow
- It is a pressure sensitive method.
- Dry and less dispersive force
- Screw arrangement
- Injection port screw arrangement
- Reverse disc applied
- Calibrate and exchange the measurement transducer

## Introduction: Extrusion of PA-66 / ScCO<sub>2</sub>



### Screw arrangement

- > Provide well mixing
- > Less degradation
- > Pressure build up



- Connect wedge die to
- Investigate mixture viscosity under
- > Different CO<sub>2</sub> uptake,
- > Temperature, pressure,
- > Shear rate.

## Introduction: viscosity measurement



### The projection and figure

$$\Delta P = \frac{K}{\tan \theta} \left( \frac{6Q}{W} \frac{2n+1}{3n} \right)^n \left[ \frac{1}{2n} \left( \frac{1}{h_2^{2n}} - \frac{1}{h_0^{2n}} \right) + \frac{1}{W(2n-1)} \left( \frac{1}{h_2^{2n-1}} - \frac{1}{h_0^{2n-1}} \right) \right]$$

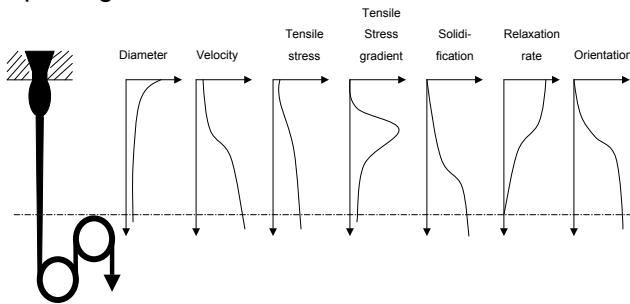
$$\eta = K \left( \frac{2n+1}{3n} \right) \left( \frac{6Q}{Wh^2} \right)^{n-1}$$

Width: 1.4 cm, θ: 0.9°

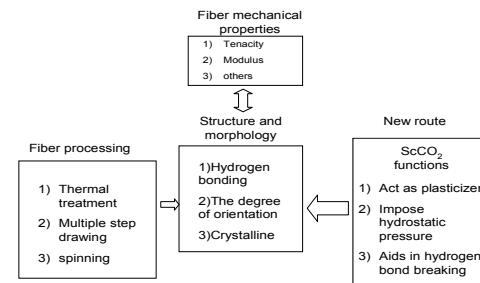
## Filament spinning and drawing



### Spinning:



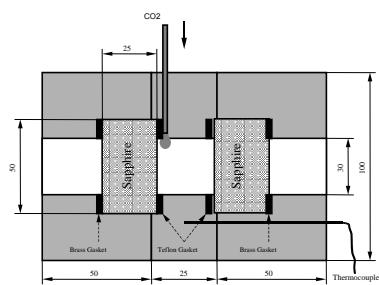
## Motivation and design concepts:



## Preliminary experiment - I



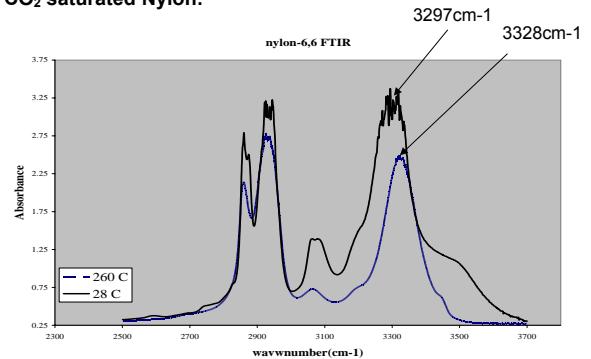
### FTIR measurement of hydrogen bond breaking process of CO<sub>2</sub> saturated Nylon:



## Preliminary experiment - I



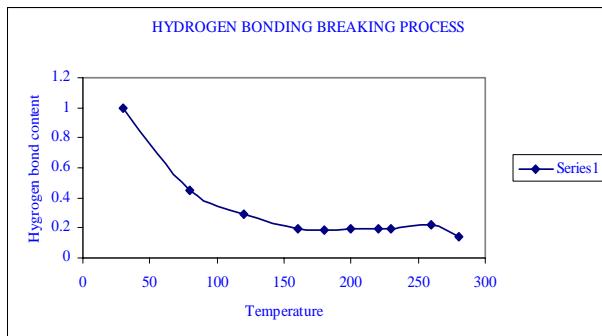
### FTIR measurement of hydrogen bond breaking process of CO<sub>2</sub> saturated Nylon:



## Preliminary experiment - I



- FTIR measurement of hydrogen bond breaking process of CO<sub>2</sub> saturated Nylon:



## Preliminary experiment - II



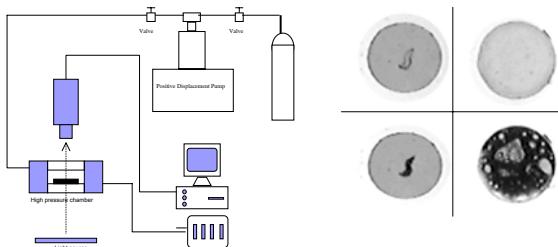
Solubility of CO<sub>2</sub> in molten Nylon-6,6:

- Motivation:
  - Injection limits of CO<sub>2</sub> during extrusion.
  - Control uptake of CO<sub>2</sub> during fiber spinning
- Swelling image analysis...

## Preliminary experiment - III



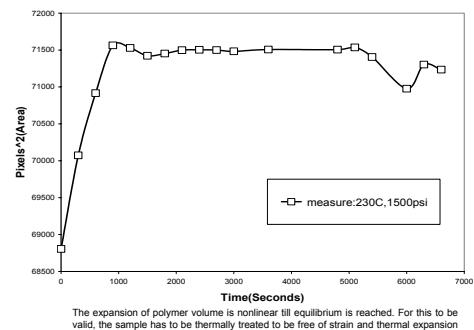
Swelling of nylon-6,6 in supercritical CO<sub>2</sub>



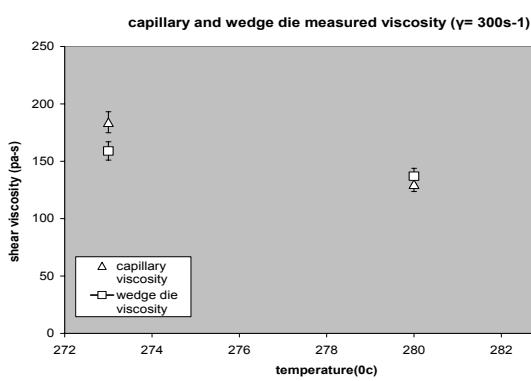
## Preliminary experiment - III



Swelling of nylon-6,6 in supercritical CO<sub>2</sub>



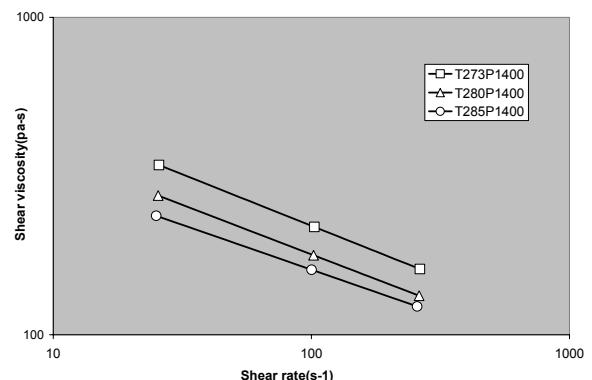
## Extrusion Results:



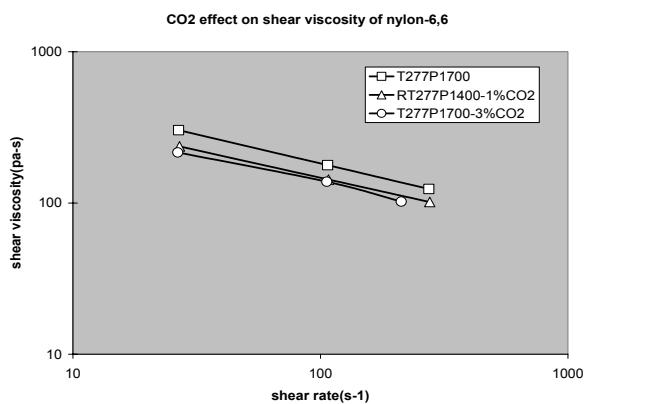
## Extrusion Results:



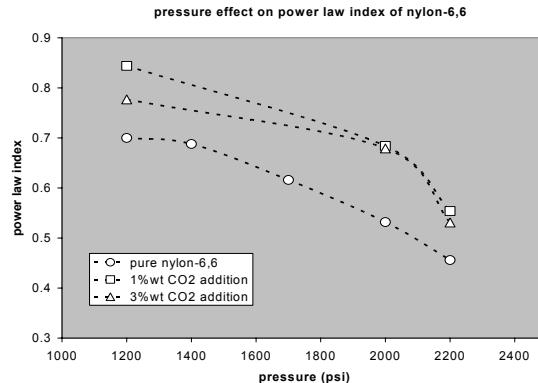
temperature effect on nylon shear viscosity(no CO<sub>2</sub>)



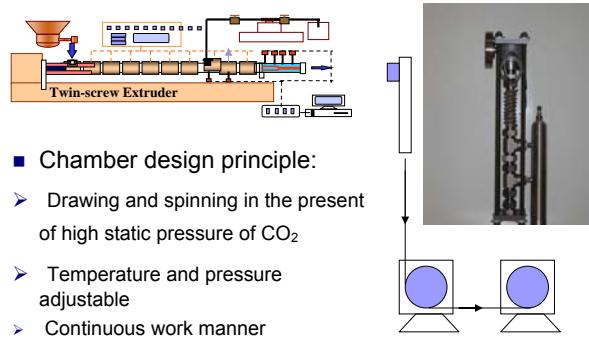
## Extrusion Results:



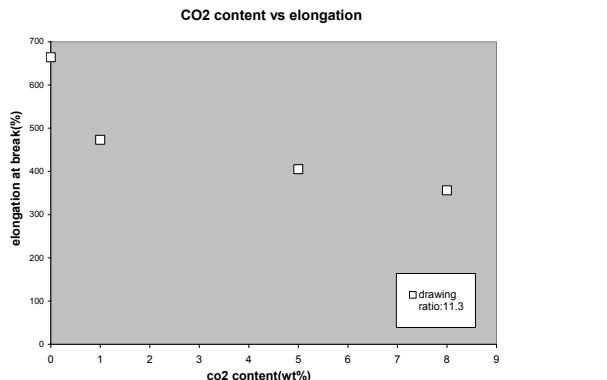
## Extrusion Results:



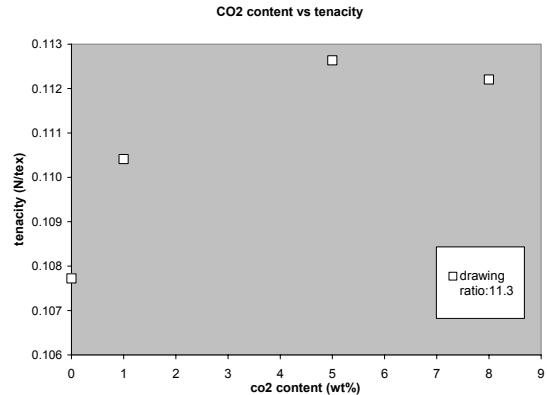
## Filament spinning of PA-66 & mixtures: set up & chamber design



## Filament spinning of PA-66 & mixtures:



## Filament spinning of PA-66 & mixtures:



## Conclusions:

CO<sub>2</sub> function as a plasticizer to:

- Reduce nylon-6,6 melt viscosity,
- And mixture viscosity is the function of shear rate, temperature, pressure and CO<sub>2</sub> uptake.
- The solubility of CO<sub>2</sub> in nylon-6,6 melt is low, partially due to the high residual hydrogen bond content in nylon-6,6 melt.

Spinning and drawing process:

- Is setting up to conduct a new route to produce fibre in the present of high hydrostatic pressure CO<sub>2</sub>
- CO<sub>2</sub> work to increase the fibers tenacity after post-drawing, but as a trade off, its elongation at break reduced

## Future work:

- Estimate solubility of CO<sub>2</sub> in molten nylon-6,6 by viscosity measurement.
- Run spin experiments at high drawing ratio.
- Investigate the effect of CO<sub>2</sub> on fibre spinnability.



## Acknowledgements:

- My sincere thanks to my supervisor, Professor Costas Tzoganakis
- Financial support from “Materials and Manufacturing Ontario” (MMO) is gratefully acknowledged.
- Donation of material from Invista is gratefully acknowledged.



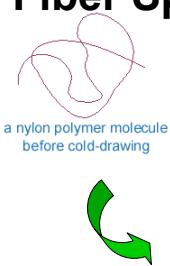
Question??



Thank you!



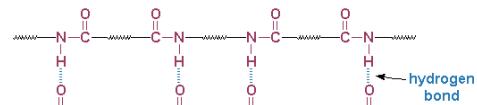
## Fiber Spinning



The nylon polymer molecules in the thin part of the filament are oriented, stretching out long and straight. This part of the filament is very strong and resists stretching.



## Fiber Spinning



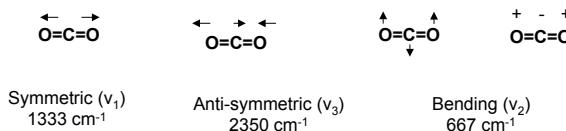
Parallel nylon chains are bound together through hydrogen bonding between amide groups.



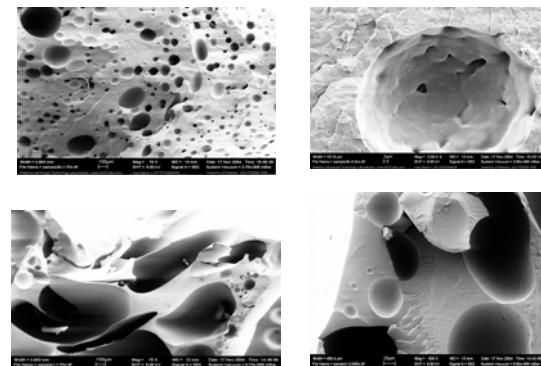
## Interactions of scCO<sub>2</sub> with Polymers



- FTIR spectroscopic studies
- Lewis acid-base interactions between CO<sub>2</sub> and electron donor species (e.g. carbonyls)



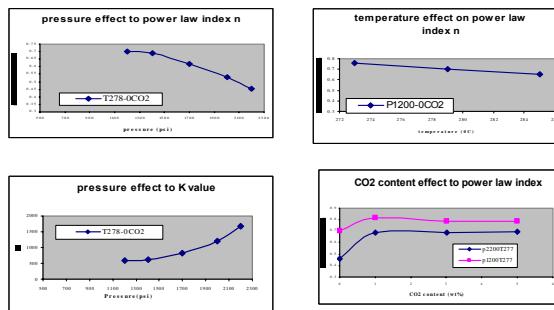
## Extrusion Results: foam structure and others



## Extrusion Results:



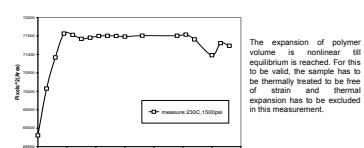
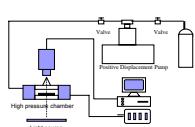
- Power law index n and K value:



Existing technologies are either too complicated to achieve or less precise:

FTIR; Gravimetric; Pressure decaying; Barometric, Volumetric, Quartz crystal Microbalance; Phase separation measurement;

## Swelling of nylon-6,6 in supercritical CO<sub>2</sub>



The expansion of polymer volume is nonlinear till equilibrium is reached. For this to happen, the polymer has to be thermally heated to be free of strain and thermal expansion has to be excluded in this measurement.

