



Innovative Steam Technologies

Power and Energy Once-Through Heat Recovery Steam Generators

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Presentation Overview

- IST Company / OTSG Origins
- OTSG technology
- OTSG Engineering Challenges
- Engineering Tools
- Innovation Enhanced Oil Recovery OTSG
- Innovation Organic Rankine Cycle OTSG
- Future Challenges





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IST Company & OTSG Origins



Company Profile



- IST founded 1992 Cambridge On, Canada
- Sales to date >200 OTSG's
- 100 staff in Design, Engineering, Manufacturing and Service
- Sales Offices Canada, Dubai, Korea







Company Profile

- Manufacturer of Once Through Steam Generator (OTSG) for the following industries:
 - Large Power Plants (Heat Recovery)
 - Manufacturing Facilities (Process Steam)
 - Small Power Plants (ORC Heat Recovery)
 - Enhanced Oil Recovery (Steam Injection)



The OTSG Origin

The Racer Program in the 1980's required a HRSG for offshore applications that was:







- Lighter
- Smaller
- Simpler
- Unaffected by the pitch and roll of the seas



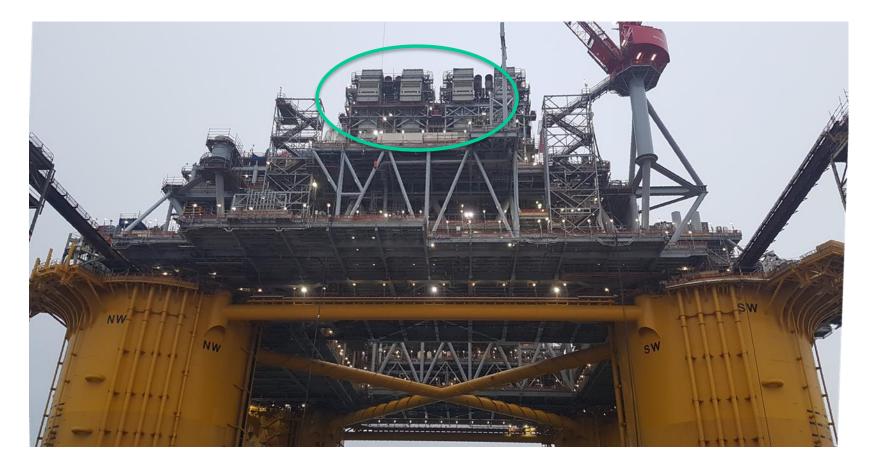
Outcome was a Once Through Steam Generator



The Result: Ultra-Modular / Compact OTSG

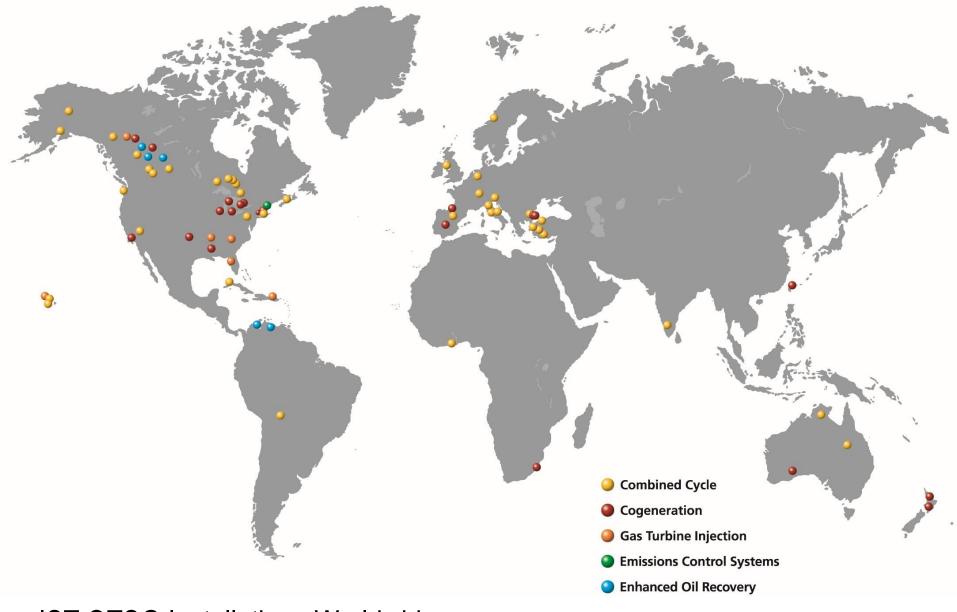


Oil Platform – OTSG Power Generation



Shell / Appomattox Platform 175,000 bpd " 2017 Shell Quality Award "





IST OTSG Installations Worldwide

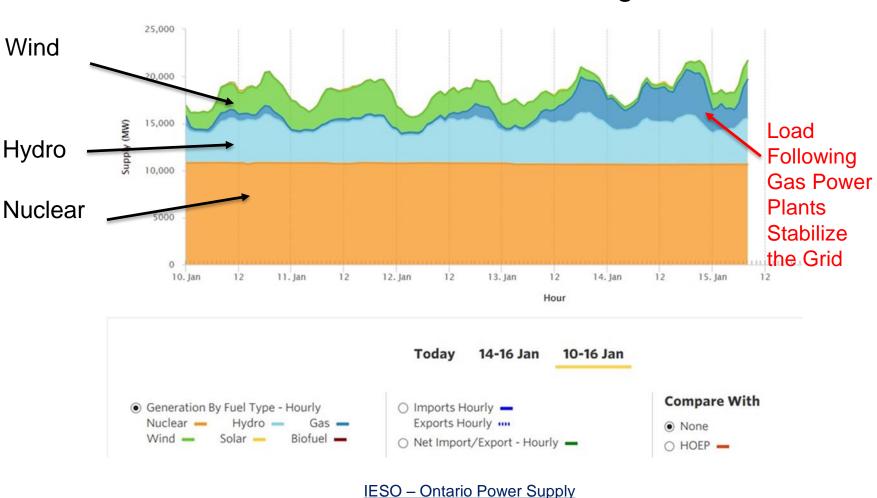






Canada (North America) Power Market

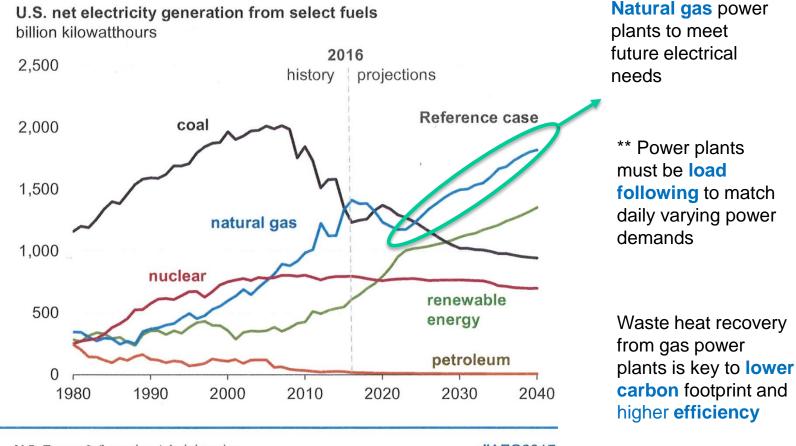
Ontario Power Generation (Daily)



Renewables and Load Following - Ontario

Power Plant Opportunities – Renewables

Natural Gas vs and Renewables



U.S. Energy Information Administration

#AEO2017





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Once Through Steam Generator (OTSG)

Introduction to HRSGs

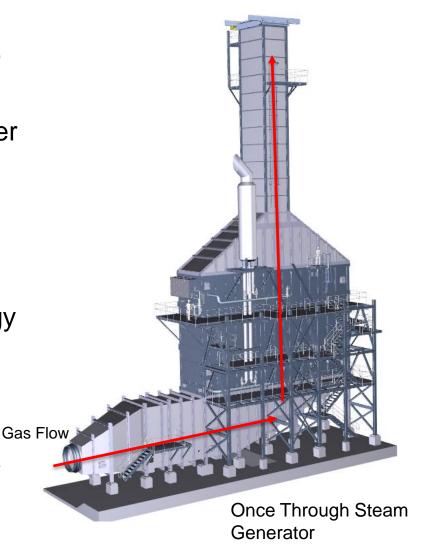
Heat Recovery Steam Generator (HRSG)

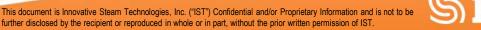
Also referred to as a waste heat boiler

 Cools hot gas – most commonly the exhaust of a gas turbine

Generates steam and regains energy

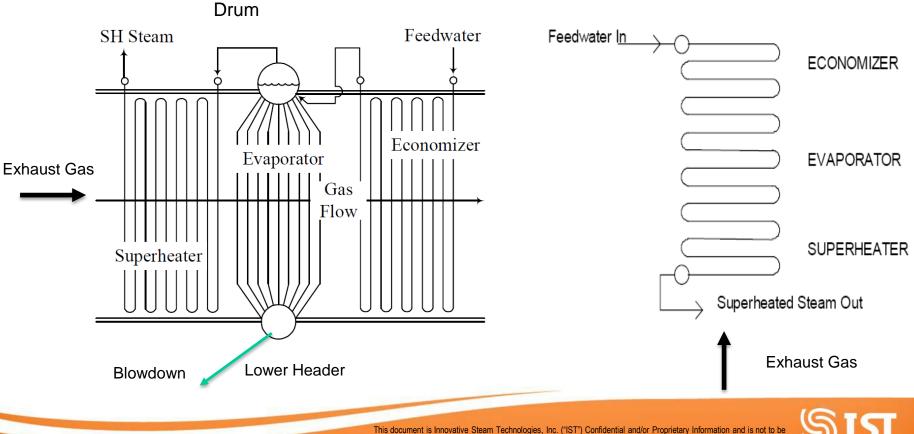
•Two main types of steam generators •Drum Boiler Ga •Once Through Steam Generator (OTSG)





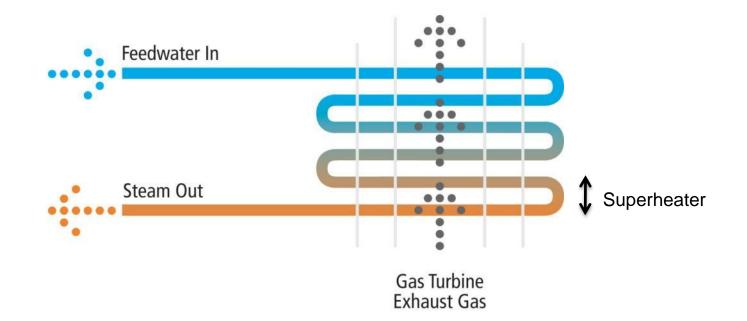
Comparison: Drum Boiler and OTSG

Drum-Type HRSG Fixed Sections OTSG Type HRSG Non Fixed Section



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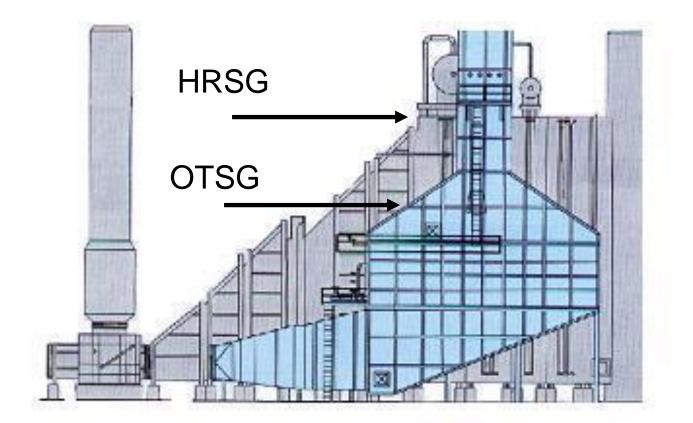
Once Through "Drumless" Design



- All tubes thin-walled → low thermal mass → fast cycling
- Compact lightweight pressure bundle
- Simple once through steam path (Water in = Water out)
- Zero Blowdown (no blowdown treatment)



OTSG vs Drum-Style HRSG



LM6000 Installation – overall size comparison



OTSG Pressure Bundle





Multiple parallel circuits 1" to 1.5" diameter tubes

Compact shop installed modules





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Engineering Challenges to Meet Market Demands

OTSG Challenges – Market Demands

Steam generation needs to aligned to varying electrical load demands. OTSGs must be:

- 1) Capable of load following Flexible steam rate operation to match required demand
- 2) Fast cold and hot starts
- 3) Augment steam production with duct firing
- 4) Emissions control (NOx and CO)



Load Following - Dry Running Capable

- Dry run gives advantages of flexible simple cycle operation with the efficiency of combined cycle operation
- "De-couples" combustion cycle from steam cycle
 - Gas turbine starts independently from the OTSG.
- Maintains gas turbine quick start capability
 - 10 minute simple cycle starts
- Offers greatest operational flexibility with large flow rate range



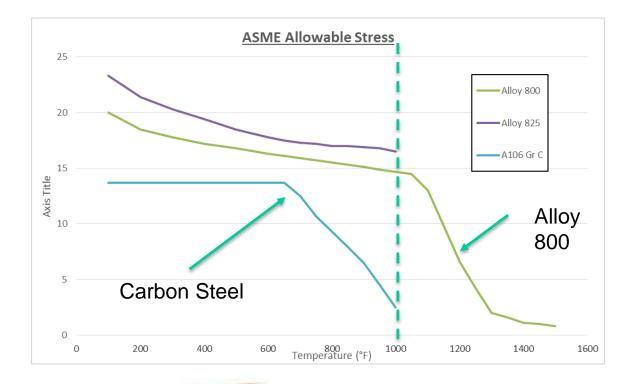


Load Following - Dry Running Capable

- OTSG capable of dry operation is designed to withstand the full gas turbine temperature (up to 1170 F). Requires special tube materials and supports.
- Materials of choice: Alloy 800 and 825 (High Nickel Chrome)
 Highly corrosion resistant and high strength

	Alloy 800	Alloy 825
Ni	30-35	38-46
Cr	19-23	19.5-23.5
Мо		2.5-3.5
Cu		1.5-3.0
Fe	39.5	22

Accommodates cold feedwater 60° F (17° C)



Load Following – FAST Start

- OTSG capable of rapid start to full load steam flow in under 15 minutes to meet grid electrical requirements
- OTSG are ideally suited for rapid start due to thin pressure tubes
- Drum boilers with thick wall steam drums requiring slow thermal ramp start.
 - Thermal fatigue is a major issue in drum boilers even with slow starts

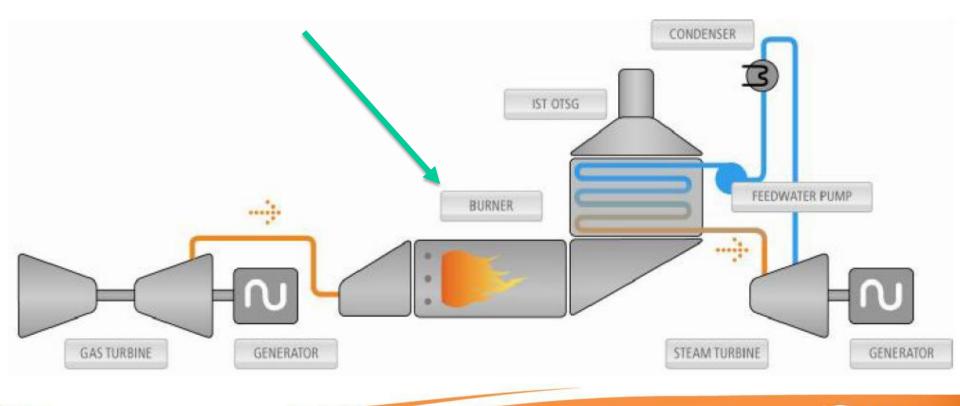


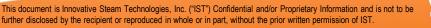
Typical Steam Drum (can be > 3" thick wall)



Steam Augmentation - Duct Burners

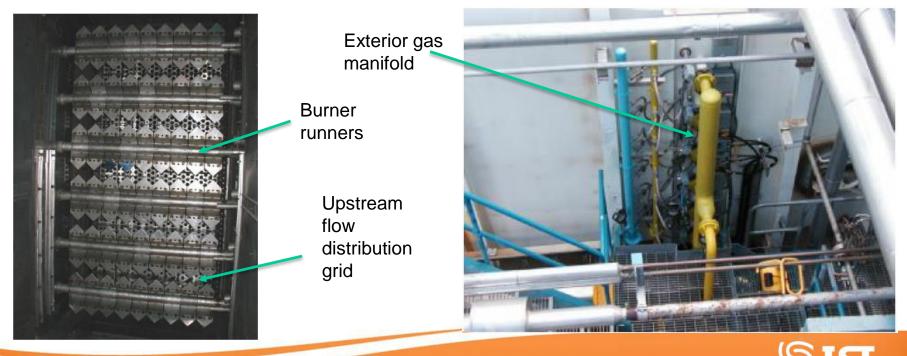
- Supplemental heat input to augment steam output and improve efficiency and meet system power demands
- Exhaust gas typically has enough oxygen (15% O2) to sustain stable combustion. Duct fired to temperature of 1200 to 1500 F.





Steam Augmentation – Why Duct Fire?

- 1. Steam demand increases without any change in the gas turbine exhaust
- 2. Insufficient heat available heat from the gas turbine to achieve steam flow
- 3. Gas turbine is completely down but steam is still needed using an auxiliary fan which replaces the GT flue gas flow (Fresh Air Firing).



Flow Distribution Grids

- Grids are used to correct turbine exhaust gas flow mal-distribution
- Variable porosity plates and turning vanes are commonly used
- Typical gas side pressure drop for a variable porosity plate ranges from 0.5" H2O to 3 inches H2O
- Must meet stringent flow uniformity requirements by burner vendors

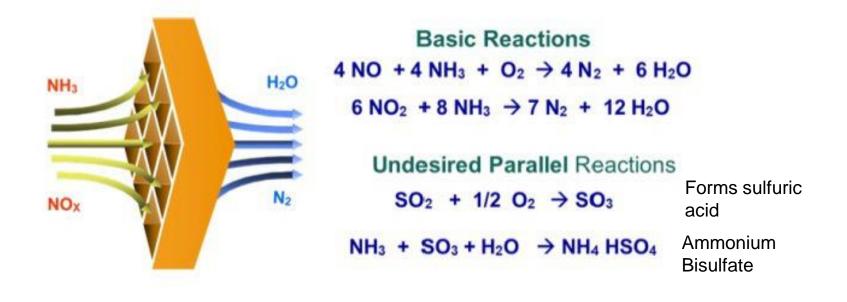




Emissions – NOx SCR Technology

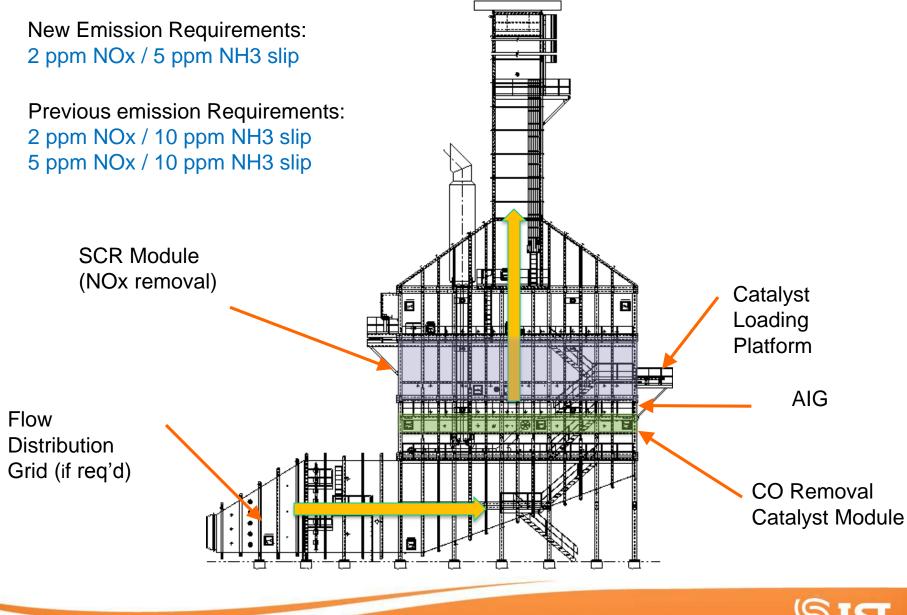
A process in which ammonia (NH_3) is injected into the gas stream containing NOx upstream of the SCR catalyst.

The gas stream then passes through the catalyst layer decomposing NOx (nitrous oxides, principally NO and NO₂) into N_2 and H_2O .

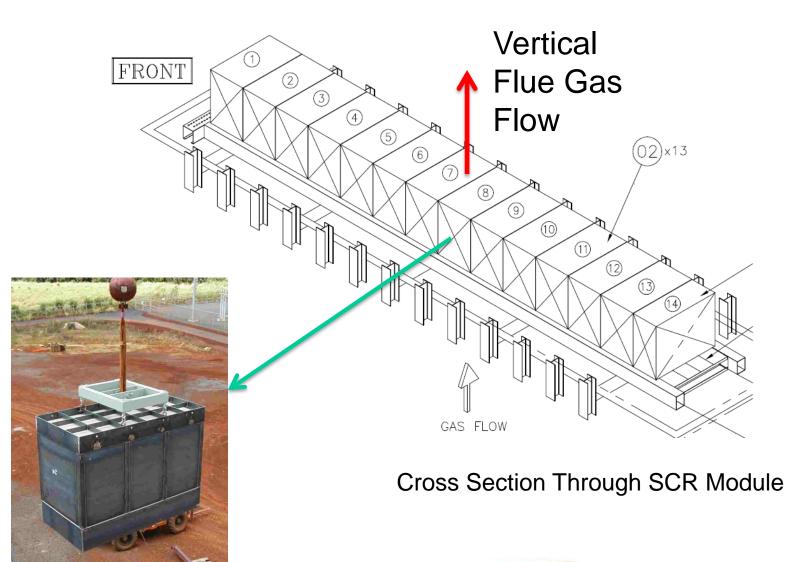




Typical Layout of OTSG w/ SCR & CO Catalysts



SCR Catalyst





Installed SCR Catalyst

- High temperature support frame
- Grating to allow for personnel walking on catalyst surface

Downstream Side View



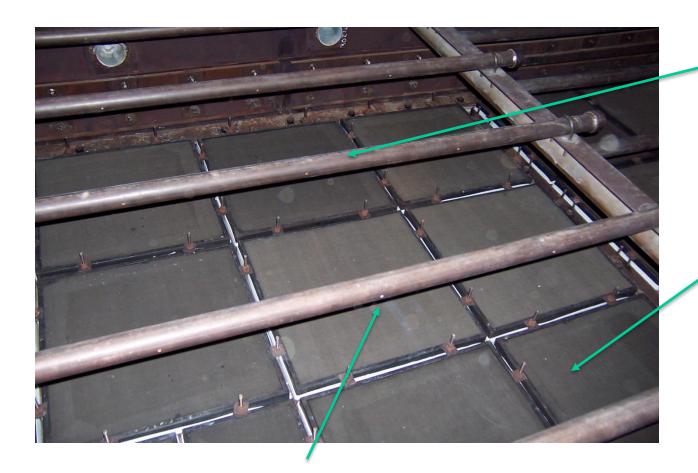


Upstream Side View

- Ti-O2-W catalyst blend on a stainless wire mesh
- Compact corrugated catalyst sheets stacked side by side
- Located in tube bundle at optimal temperature 700-750F



Ammonia Injection Grid (AIG)



Injection pipes (1.5" to 3" NPS) with drilled holes

Upstream CO catalyst (Platinum)

Ammonia injection holes





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Engineering Tools

Engineering Tools

Computer simulations play an important role in the OTSG design.

Finite Element Analysis (FEA) – Calculation of pressure part and structural member stresses, deflection, loads

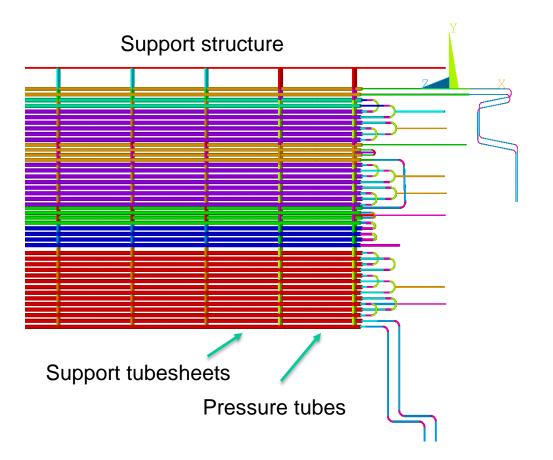
Computational Fluid Dynamics (CFD) – Calculations of flow velocities, temperature, concentrations



FEA- Loads / Stresses / Deflections

Finite Element Analysis is an important tool used to understand:

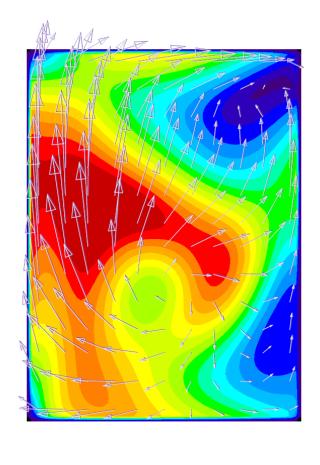
- Thermal expansion of tubes and supports
- 2. Operating stresses and design margins
- 3. Support and restraint loads

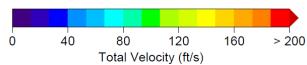


- ANSYS FEA software
- Tube row by row gas and metal temperatures are imported for accurate representation



CFD - Turbine Exhaust Profile





- Turbine exhaust is highly nonuniform flow and temperature profile.
- The flow vectors often include a swirl characteristic
- Flow velocity contour plots can range over wide range

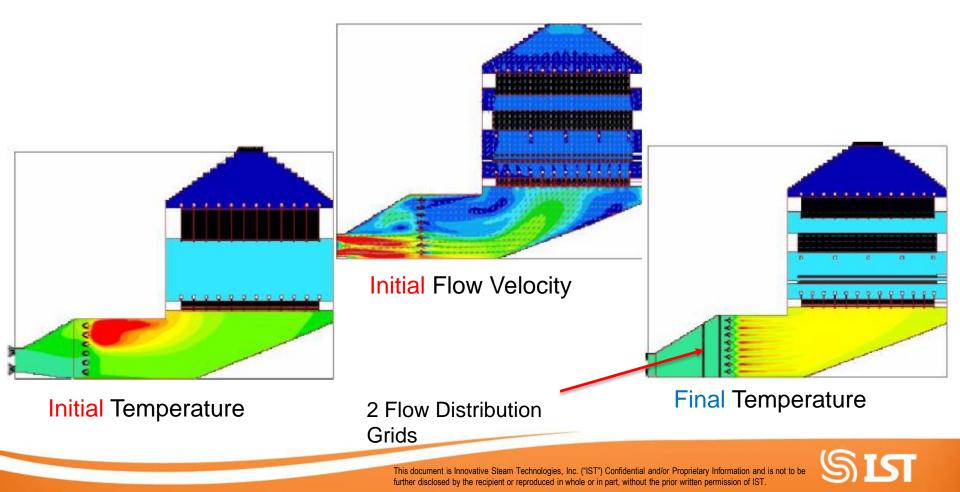
What does this mean?

Flow distribution devices are a necessity to smooth out flow into the OTSG



Flow Modelling – Horizontal Flow Arrangement

- Gas flow distribution leaving the gas turbine is non-uniform
- Proper performance of the HRSG, duct burner and emission equipment requires uniform flow and temperature profile



Combustion Modelling – Flame

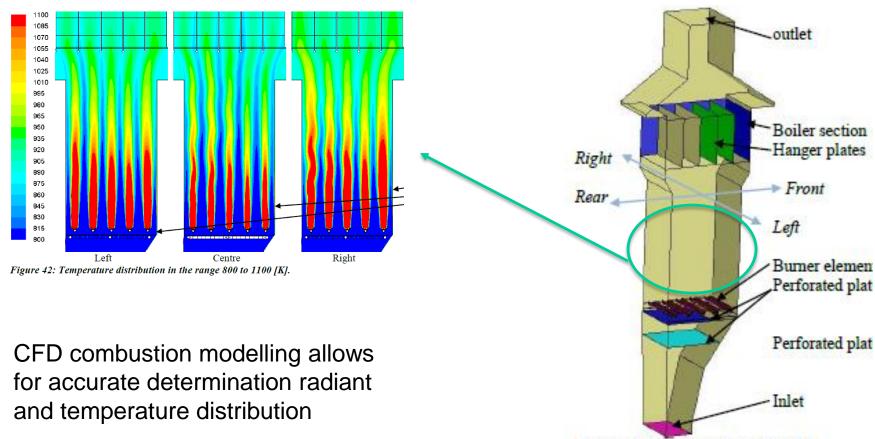
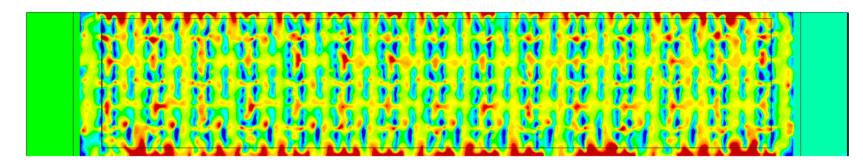


Figure 1 Shaded outline of model



CFD– SCR Ammonia Modelling

- Confirm AIG hole pattern creates a uniform ammonia distribution from each lance pipe
- Dispersion CFD modelling to ensure ammonia injected by AIG piping is uniform at SCR inlet face
- Important to meet uniform NH3 / NOx distribution



Ammonia mass distribution upstream of SCR before optimization





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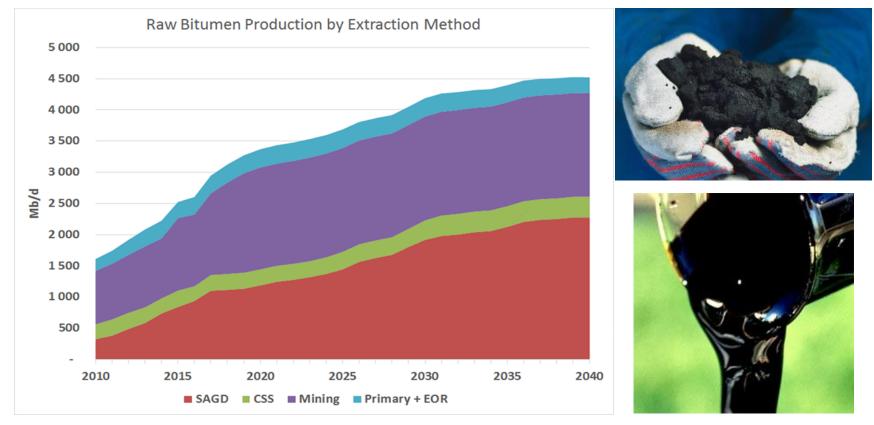
Innovation – Key to Develop New Markets





Innovation Enhanced Oil Recovery OTSG

Current Climate – NEB (National Energy Board)



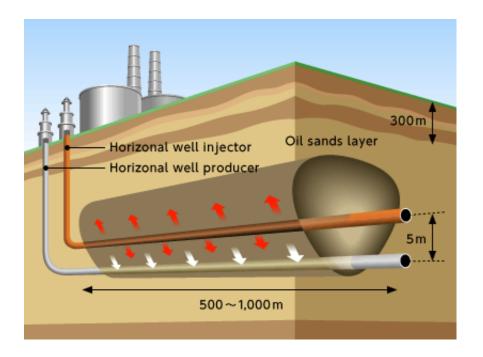
National Energy Board recently released Canada's Energy Future 2017 Supplement

- Remaining 80% of oil sands only accessible using in-situ methods
- Steam injection is the primary proven method to recover oil/bitumen



Enhanced Oil Recovery (EOR)

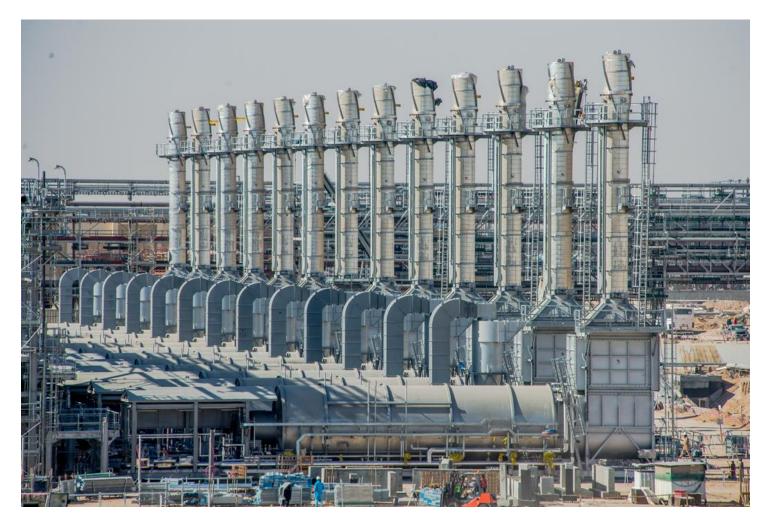
ALBERTA : Steam Assisted Gravity Drainage (SAGD)



OTSGs provides the majority of steam for EOR worldwide!



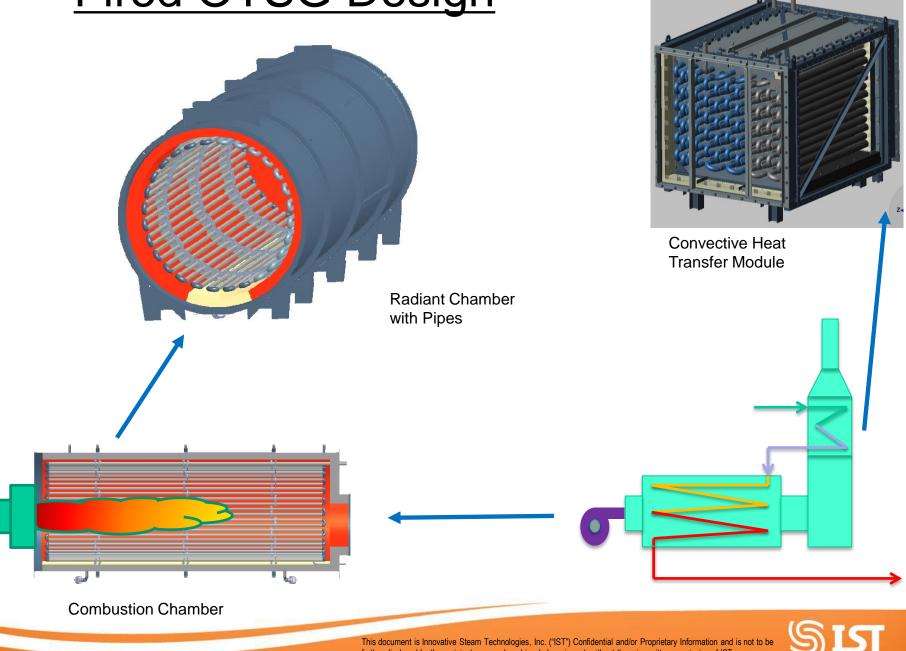
EOR OTSG



Petrofac/ Lower FARS 60,000 Barrels Oil / Day



Fired OTSG Design



OTSG Inlet Water Quality

Extremely high Total Dissolved Solids (TDS) is unique to EOR OTSGs

		Maximum	
Constituent	Unit	Limit	
Total Silica	ppm	50	
Total Iron	ppm	0.05	
Hydrogen Sulfide	ppm	0	
Total Acidified Hardness (as CaCO3) - Normal			
(Excursion)	ppm	0.2 (0.5)	
Total Alkalinity	ppm	<2000	
Total Dissolved Solids	ppm	<8000	
Total Organic Carbon	ppm		
Total Suspended Solids	ppm	1	
Oil & Grease	ppm	0.5	
Turbidity	NTU	2	
рН	pН	>9.3	
Oxygen	ppb	5	



Steam Blowdown Water

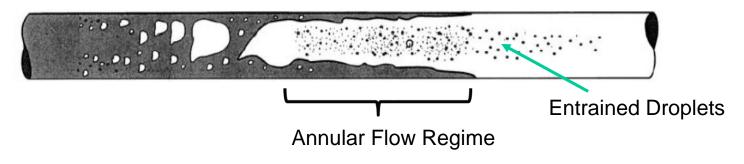
OTSG must produce wet steam to carry through BFW dissolved solids!



Industry Standard

• OTSG radiant piping outlet operates under **annular** flow regime

Dry Spots Lead to Deposits



- A **layer of water** on the pipe surface absorbs incoming radiant energy (steam core with droplets)
- Water impurities are carried through in steam water content.
- KEY to maintain water contact on the pipe surface
- Industry standard Operate 75 to 80% steam quality based on proven reliable experience

IST SQ90[™] Solution to Higher Steam Quality

- Internally Rifled Pipes:
 - Maintains all water on pipe surface and equalize water impurity concentrations
- The internal surface has a series of raised ribs that imparts a rotational fluid flow
- The centrifugal force pushes all entrained water equally around pipe perimeter
- Operates at 90% steam quality (an industry first !)

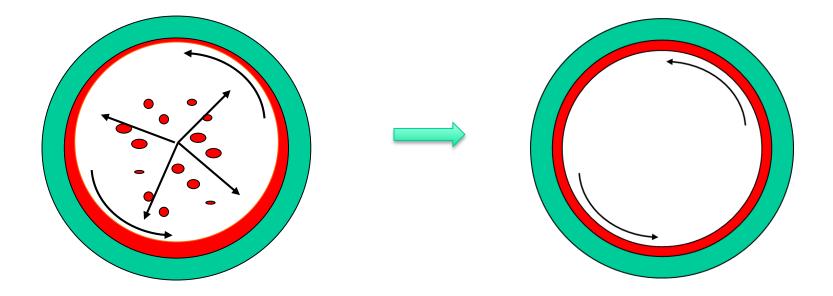


Inside Rifled Pipe

The SQ90[™] OTSG design is **patented in Canada, US and GCC (pending)**



IST SQ90[™] Solution to Higher Steam Quality



Uniform Surface Water Film = Ability for High Steam Quality





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Innovation Organic Rankine Cycle OTSG

Organic Rankine Cycle (ORC)

- Many small gas turbines and generators are run in simple cycle
 - An opportunity exists for improved system efficiency
 - However, at existing sites there is rarely a local use for the heat
- US Department of Energy estimates there are 1.5 to 2.0 quadrillion BTU/hr with gas temperature < 500 F from industrial gas streams. A HUGE potential for carbon reduction!
- Smaller gas turbines have insufficient heat available for heat recovery using steam making the system inefficient.
 - Switch to organic fluids (ie. R245fa) for heat recovery and electricity generation (Referred to Organic Rankine Cycle (ORC) process)
- ORC application: Gas temperature less than 800 F (427 C)



TransGas Rosetown Project Example

- Natural gas compressor station in southwestern Saskatchewan
- Compressor driven by Solar Centaur Gas Turbine (4500 HP)



Turboden: ORC turbine / regenerator / generator

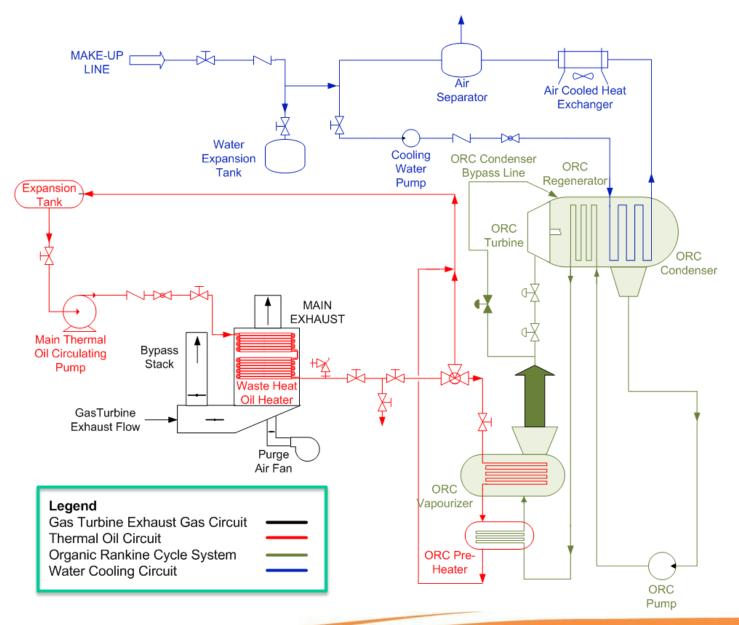


 IST supplied an EPC turnkey 1MWe power plant utilizing waste heat from the Solar Centaur GT (800 F flue gas temperature)



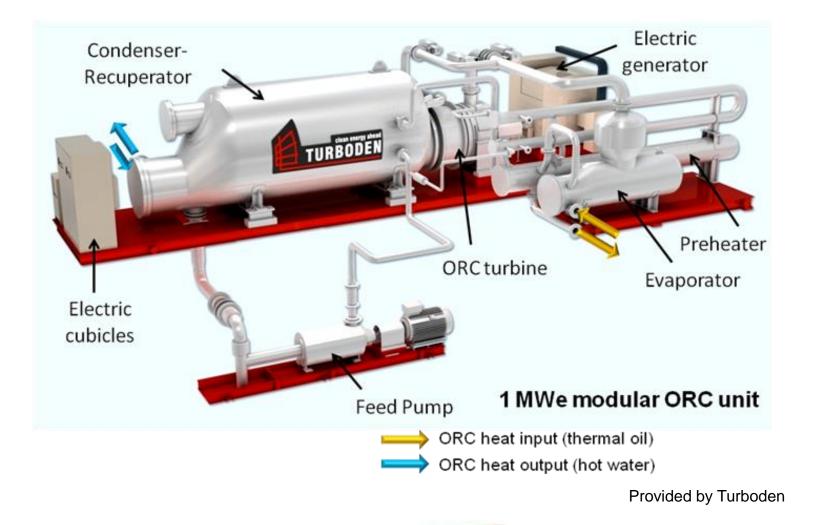


ORC - Process Flow Diagram

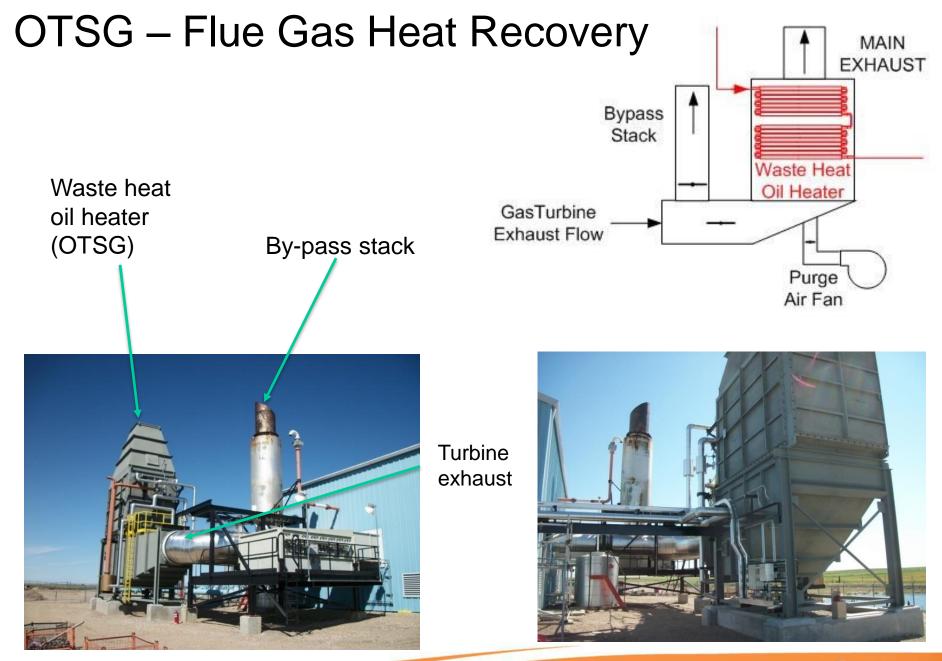




ORC Plant Layout









ORC Advantages

ORC Challenges

- Organic working fluid has low boiling point (Efficient).
- Fully automated plants
- Low system operating pressure (Safe)
- High molecular weight working fluid
 - Low speed turbines that increase the system reliability and efficiency.
- 'Dry fluids': Vapour always leaves the turbine in a superheated condition.
 - No risk of damaging turbine with liquid.

- High installed costs often makes projects prohibitive. Must have installed costs <\$5000/kWe
- Feasible only for regulated electricity markets with high electrical sell costs (> \$0.16 /kW-hr)
- Expensive organic fluid replacement costs
- Most economical solutions begin at 1MWe and higher. Leaves behind a large untapped market.



ORC Innovation Next Steps....

• Direct evaporation of organic working fluid in the turbine or reciprocating engine flue gas.

Challenge: Overheating H245fa can form hydrofluoric acid

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- Eliminate thermal oil transfer loop reduces cost and increases overall efficiency
- Completely modular design to minimize field erection costs
- Turbo expander cost reduction

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Future Challenges

Canada Future Challenges

Electrical producers maintaining competitiveness in a carbon tax environment

Development of low cost CAPEX and OPEX CO2 capture technology

 Suppressed oil prices and carbon tax making Canada's oil sands industry unprofitable

Lack of investment in today's market

Reduced NOx emissions

Challenges to achieving sub 2 ppm NOx

 Development of more cost effective Organic Rankine Cycle heat recovery

CAPEX costs need to be driven down





End Questions?

once through steam generator